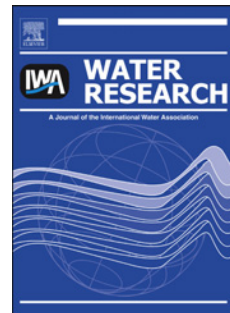


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1 **Occurrence, partition and removal of pharmaceuticals in sewage water**
2 **and sludge during wastewater treatment**

3

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24 **Abstract**

25

26 During 8 sampling campaigns carried out over a period of two years, 72 samples, including
27 influent and effluent wastewater, and sludge samples from three conventional wastewater
28 treatment plants (WWTPs), were analyzed to assess the occurrence and fate of 43
29 pharmaceutical compounds. The selected pharmaceuticals belong to different therapeutic
30 classes (i.e. analgesics and anti-inflammatory drugs, anti-ulcer agent, psychiatric drugs,
31 antiepileptic drug, antibiotics, β -blockers, diuretics, lipid regulator and cholesterol lowering
32 statin drugs). The obtained results showed the presence of 32 target compounds in
33 wastewater influent and 29 in effluent, in concentrations ranging from low ng/L to a few
34 $\mu\text{g/L}$ (e.g. antiinflammatories). The analysis of sludge samples showed that 21
35 pharmaceuticals accumulated in sewage sludge from all three WWTPs in concentrations up
36 to 100ng/g. This indicates that even good removal rates obtained in liquid phase (i.e.
37 comparison of influent and effluent wastewater concentrations) do not imply degradation to
38 the same extent. For this reason, the overall removal was estimated as a sum of all the
39 losses of a parent compound produces by different mechanisms of chemical and physical
40 transformation, biodegradation and sorption to solid matter. The target compounds showed
41 very different removal rates and no logical pattern in behavior even if they belong to the
42 same therapeutic groups. What is clear is that the elimination of most of the substances is
43 incomplete and improvements of the wastewater treatment and subsequent treatments of the
44 produced sludge are required to prevent the introduction of these micro-pollutants in the
45 environment.

46

47 **Keywords:** pharmaceuticals, wastewater treatment, wastewater, sludge, removal rate

48 **1. Introduction**

49

50 Pharmaceuticals are a large and diverse group of compounds designed to prevent,
51 cure and treat disease and improve health. They have long been used in significant
52 quantities throughout the world. Their usage and consumption are increasing consistently
53 due to the discoveries of new illnesses and drugs, the expanding population and the
54 inverting age structure in the general population, as well as due to expiration of patents with
55 resulting availability of less expensive generics (Daughton, 2003). After intake, these
56 highly active compounds undergo metabolic processes in organism. Significant fractions of
57 the parent compound are excreted in unmetabolized form or as an active metabolite to raw
58 sewage and wastewater treatment systems. Sewage treatment plant effluents are discharged
59 to water bodies or reused for irrigation, and biosolids produced are reused in agriculture as
60 soil amendment or disposed to landfill. Thus body metabolization and excretion followed
61 by wastewater treatment is considered to be the primary pathway of pharmaceuticals to the
62 environment.

63 Continual improvements in analytical equipment and methodologies enable
64 measuring of pharmaceuticals at lower and lower concentration levels in different
65 environmental matrices. Pharmaceuticals and their metabolites in surface waters and
66 aquatic sediment were subject of numerous studies about pharmaceuticals in the
67 environment (Pérez et al., 2007; Bartelt-Hunt et al., 2009; Grujic et al., 2009; Khetan et al.,
68 2007; Miller et al., 2008; Nilsen, 2007; Gros et al., 2006; Hernando et al., 2006; Ellis,
69 2006; Vazquez-Roig et al., 2010). Several studies investigated occurrence and distribution
70 of pharmaceuticals in soil irrigated with reclaimed water (Gielen et al., 2009; Ternes et al.,

71 2007; Kinney, 2006)) and soil that received biosolids (Carbonell et al., 2009; Sabourin et
72 al., 2009; Lapen et al., 2008; Topp et al., 2008) from urban sewage treatment plants.
73 Results of these studies indicated that wastewater treatment plants are not enough efficient
74 to remove these micropollutants from wastewaters so they find their passage to the
75 environment. Once entered the environment, pharmaceutically active compounds can
76 produce subtle effects on aquatic and terrestrial organisms, especially on the former since
77 they are exposed to long term exposure by wastewater effluents. Several studies
78 investigated and reported on it (Schnell et al., 2009; Pomati et al., 2006; Cleuvers, 2004;
79 Laville et al., 2004; Nentwig et al., 2004).

80 Therefore, the occurrence of pharmaceutical compounds and the extent to which
81 they can be eliminated during wastewater treatment have become active subject matter of
82 actual research. Conventional systems that use an activated sludge process are still widely
83 employed for wastewater treatment, mostly because they produce an acceptable quality
84 effluent at reasonable operating and maintenance costs. But this type of treatment has
85 limited capability of removing pharmaceuticals from wastewater (Kasprzyk-Hordern et al.,
86 2009; Gros et al., 2010; Wick et al., 2009). Most of the studies on the fate of
87 pharmaceuticals in WWTPs focused only on aqueous phase, and concentrations of the
88 compounds in sludge were rarely determined mainly due to the demanding efforts required
89 in the analysis in this difficult matrix. Out of 117 publications studied by Miege et al
90 (Miège et al., 2009), only 15 reported the concentrations of pharmaceuticals in sludge and 1
91 in suspended solid, and none of these papers reported removal obtained taking into account
92 both liquid and solid phases of WWTPs. The screening of sewage sludge showed that these
93 micropollutants are very present in this medium (Radjenovic et al., 2009; McClellan et al.,
94 2010; Okuda et al., 2009; Díaz-Cruz et al., 2009; Lillenberg et al., 2009; Nieto et al., 2009).

95 In this study we aimed to determine the contamination of wastewater and sludge
96 with 43 pharmaceutical compounds in order to obtain more in-depth information on their
97 fate during conventional wastewater treatment. The selected pharmaceuticals belong to
98 different therapeutic groups (i.e. analgesics and anti-inflammatory drugs, anti-ulcer agent,
99 psychiatric drugs, antiepileptic drug, antibiotics, β -blockers, diuretics, lipid regulator and
100 cholesterol lowering statin drugs, anti-histamines). The samples were provided from three
101 conventional full-scale activated sludge sewage treatment plants with anaerobic digestion
102 of sludge, from the region of Catalonia (Spain). The preparation and analysis of the samples
103 were performed using high performance liquid chromatography coupled to a hybrid triple
104 quadrupole – linear ion trap mass spectrometer (HPLC-QLIT- MS/MS) according to the
105 previously developed multi-residual methodologies for analysis of pharmaceuticals in
106 wastewater and sludge samples (Gros et al., 2009; Jelic et al., 2009).

107

108 **2. Experimental part**

109 **2.1. Chemicals**

110

111 All the pharmaceutical standards for target compounds were of high purity grade
112 (>90%). Ibuprofen, Naproxen, Ketoprofen, Diclofenac and Gemfibrozil were supplied by
113 Jescuder (Rubí, Spain). Acetaminophen, Indomethacin, Mefenamic acid, Phenazone,
114 Bezifibrate, Mevastatin, Fenofibrate, Pravastatin (as sodium salt), Carbamazepine,
115 Famotidine, Ranitidine (as hydrochloride), Cimetidine (as hydrochloride), Erythromycin
116 (as hydrate), Azithromycin (as dehydrate), Roxitromycin, Clarithromycin, Josamycin,
117 Tylosin A, Sulfamethazine, Trimethoprim, Chloramphenicol, Atenolol, Sotalol, Metoprolol

118 (as tartrate), Timolol, Pindolol, Nadolol, Salbutamol, Clenbuterol (as hydrochloride),
119 Enalapril (as maleate), Glibenclamide, Furosemide, Hydrochlorothiazide and
120 Metronidazole were purchased from Sigma-Aldrich (Steinheim, Germany). Standard
121 Atorvastatin (as calcium salt) was provided by LGC Promochem (London, UK), while
122 Diazepam, Lorazepam and Butalbital were from Cerilliant (Texas, USA).

123 The isotopically labelled compounds, used as internal standards, were
124 Sulfamethazine-d₄, Famotidine-¹³C₃, rac-Timolol-d₅ maleate, Clarithromycin-N-methyl-d₃,
125 Atorvastatin-d₅ sodium salt, Fenofibrate-d₆, Metoprolol-d₇, Metronidazole hydroxyl-d₂,
126 Pravastatin-d₃, Ketoprofen-¹³CD₃, Indomethazine-d₄, rac-Naproxen-d₃, Mefenamic acid-d₃,
127 Gemfibrozil-d₆, Bezafibrate-d₄ and Furosemide-d₅ from Toronto Research Chemicals;
128 Diazepam-d₅ and Phenobarbital-d₃ from Cerilliant (Texas, USA); Atenolol-d₇,
129 Carbamazepine-d₁₀, Ibuprofen-d₃, Clotrimazole-d₅, Enalapril-d₅, Hydrochlorothiazide-d₂,
130 Glyburide-d₃, Albuterol-d₃, Cimetidine-d₃, Antipyrine-d₃, Acetaminophen-d₄, Diclofenac-
131 d₄, Clofibrac-d₄ acid, Hydrochlorothiazide-3,3-d₂ from CDN Isotopes (Quebec, Canada);
132 Sotalol hydrochloride d₆ from Dr. Ehrenstorfer (Augsburg, Germany) and Erythromycin-
133 ¹³C₃, d₃ (N-Methyl-¹³C₃, d₃) from Isotec (Ohio, USA).

134 The solvents, HPLC grade methanol, acetonitrile, water (Lichrosolv) and formic
135 acid 98% were provided by Merck (Darmstadt, Germany). Nitrogen used for drying from
136 Air Liquide (Spain) was of 99.995 % purity.

137 The cartridges used for solid phase extraction were Oasis® HLB (200mg, 6mL)
138 from Waters Corporation (Milford, MA, USA). The syringe filters of 0.45µm pore size
139 were purchased from Pall Corp (USA).

140 The individual standard solutions as well as isotopically labelled internal standard
141 solutions were prepared on a weight basis in methanol. Furosemide and Butalbital were

142 obtained as solutions in acetonitrile, while Lorazepam and Diazepam were dissolved in
143 methanol, at a concentration of 1 mg/mL. The solutions were stored at -20°C. Fresh stock
144 solutions of antibiotics were prepared monthly due to their limited stability while stock
145 solutions for the rest of substances was renewed every three months. A mixture of all
146 pharmaceuticals was prepared by appropriate dilution of individual stock solutions in
147 methanol-water (25:75, v/v) and it was renewed before each analytical run. A separate
148 mixture of isotopically labelled internal standards, used for internal standard quantification,
149 was prepared in methanol and further diluted in methanol-water (25:75, v/v) mixture.

150

151 **2.2. Sample collection**

152

153 Samples (i.e. influent and effluent wastewater, and sewage sludge) were obtained
154 from three full-scale wastewater treatment plants (WWTPs) in the region of Catalonia
155 (Spain). All the samples were collected in eight sampling campaigns between July 2007
156 and March 2009, in campaign intervals of 2 to 3 months. Composite influent and effluent
157 waste water samples (24h) were collected in 1L amber glass bottles and kept on 4°C until
158 extraction (within 48 hours). Prior to extraction, the water was vacuum filtered through
159 1µm glass fiber filters, followed by 0.45µm nylon membrane filters (Teknokroma,
160 Barcelona, Spain). Sludge samples were freeze-dried (LioAlfa 6, Telstar) at -50 °C and
161 under 0.044 bar vacuum and stored at -20 °C until the analysis.

162

163 Composite wastewater samples were collected at the entrance of the treatment plant
164 i.e. influent wastewater and at the exit of the plants i.e. effluent wastewater (after the
secondary treatment at WWTP2 and WWTP3, and after the tertiary one in WWTP1). The

165 analyzed samples of sludge were collected at the final phase of the process, i.e. treated
166 sewage sludge.

167 In Table 1 are summarized some characteristics of the three investigated wastewater
168 treatment plants. WWTP1 and WWTP2 treat predominantly municipal waste water, while
169 the WWTP3 influent has an important industrial contribution. The WWTP1 is designed for
170 210000 equivalent inhabitants (eq.inh.) and to treat up to 47500 m³/day of wastewater. It is
171 situated in the tourist coastal area where the amount and the quality of water entering the
172 plant are significantly affected by the seasonal population growth. The wastewater flow in
173 WWTP1 changes from 15000, during the winter months, to 32000 m³/day during the
174 summer months. The WWTP 2 can treat up to 35000m³/day of wastewater serving a
175 population equivalent of around 170000. It usually works with 80% of designed treatment
176 capacity, with fairly constant flow rate of water of approx.25000 m³/day (in 2009). The
177 WWTP3 treated an average of 25000m³/day in 2008, which is about 80% of the total
178 treatment capacity of the plant. The wastewater treatments in all the plants include primary
179 and secondary treatment, and in the case of WWTP1 an additional tertiary treatment. The
180 plants employ biological activated sludge process for wastewater treatment. Sludge
181 generated during primary and secondary treatment is thickened and blended and fed to
182 anaerobic digester system in WWTP2 and WWTP3 and, in the case of the WWTP1,
183 centrifuged and sent to composting.

184

185 **2.3. Sample preparation**

186

187 Procedures for preparation of water and sludge samples for instrumental analysis
188 were described in detail previously (Gros et al., 2009; Jelic et al., 2009).

189 In brief, in the filtered-aliquots of wastewater (100ml for influent and 200ml for
190 effluent) Na₂EDTA was added to a concentration of 0.1vol%. Then the target compounds
191 were separated by solid phase extraction (Oasis HLB cartridges, 6 cc, 200 mg; Waters
192 Corp., Milford, MA) using a Baker vacuum system (J.T. Baker, Deventer, The
193 Netherlands), and concentrated via elution with pure methanol. The 8ml eluents were
194 evaporated under a stream of nitrogen and reconstituted in a methanol-water mixture
195 (25:75). Prior to instrumental analysis, these samples were fortified by a mixture of internal
196 standard to a final concentration of 20ng/ml.

197 Sludge samples were extracted using an accelerated solvent extraction (ASE)
198 (Dionex ASE 200, Dionex; Sunnyvale, CA). The extractions were carried out using a
199 methanol-water mixture (1:2) as extraction solvent, at 1500 psi and 100 °C in 3 static
200 cycles, each lasting 5 minutes. Finally, the cell was flushed with 100% cell volume of fresh
201 solvent. Concentrated extracts were dissolved in water in order to reduce the content of
202 methanol (< 5 vol%) and processed further as water samples. Instrumental analysis of all
203 samples was done by HPLC-QLIT-MS/MS.

204

205 **2.4. Instrumental analysis**

206

207 The analytical method used in this study was already developed by M. Gros et al
208 (Gros et al., 2009). Samples were analysed using high performance liquid chromatography
209 (HPLC) coupled to tandem mass spectrometry (MS/MS). LC analysis was performed using
210 Symbiosis™ Pico (SP104.002, Spark, Holland), equipped with an autosampler and
211 connected in series with a 4000 QTRAP Hybrid Triple Quadrupole - Linear Ion Trap mass
212 spectrometer equipped with a Turbo Ion Spray source (Applied Biosystems-Sciex, Foster

213 City, CA, USA). Chromatographic separation was achieved with a Purospher Star RP-18
 214 endcapped column (125mm x 2.0 mm, particle size 5 μ m) preceded by a C₁₈ guard column
 215 (4 x 4, 5 μ m), both supplied by Merck (Darmstadt, Germany).

216 The mobile phases for the analysis in negative ionization (NI) mode were a mixture
 217 of acetonitrile-methanol (1:1, v/v) (i.e. eluent A), and HPLC grade water (i.e. eluent B).
 218 The analysis in positive ionization (PI) mode was performed using acetonitrile as eluent A
 219 and HPLC grade water with 0.1% formic acid as eluent B. The target compounds were
 220 scanned in MRM, monitoring two transitions between the precursor ion and the most
 221 abundant fragment ions for each compound. Further information on the methodology and
 222 its performances can be found elsewhere (Gros et al., 2009; Jelic et al., 2009).

223

224 2.5. Removal rate calculation

225

226 In this study we employed a mass balance approach in order to assess quantitatively
 227 the removal of the selected pharmaceuticals during wastewater treatment. Even when
 228 dealing with such a complex system, we can assume that the WWTP behaves as a black-
 229 box with only one entrance (i.e. influent water) and two outlets (i.e. effluent water and
 230 treated sludge) and operates at steady state over the studied period of two years. Then, from
 231 the measured concentrations and the operation parameters (i.e. flow rates of influent,
 232 $\dot{V}_{influent}$, and effluent, $\dot{V}_{effluent}$, and sludge production, \dot{P}_{sludge}) could be written as follows:

$$233 \quad \dot{R}_{Overall} = \dot{m}_{in} - \dot{m}_{out} \quad (1)$$

$$234 \quad \dot{m}_{in} = \dot{m}_{influent} \quad (2)$$

$$235 \quad \dot{m}_{out} = \dot{m}_{effluent} + \dot{m}_{sludge} \quad (3)$$

$$236 \quad \dot{V}_{influent} = \dot{V}_{effluent} = \dot{V}_l \quad (4)$$

$$237 \quad \dot{R}_{Overall} = c_{influent} \times \dot{V}_l - (c_{effluent} \times \dot{V}_l + c_{sludge} \times \dot{P}_{sludge}) \quad (5)$$

238

239 where \dot{m}_{in} , \dot{m}_{out} , $\dot{m}_{influent}$, $\dot{m}_{effluent}$ and \dot{m}_{sludge} are the mass flow rate (in g/day) of
 240 inlet, outlet, influent liquid, effluent liquid and sludge, respectively. $\dot{R}_{Overall}$ (g/day) is the
 241 mass load lost per unit of time due to the sum of all processes that can occur during
 242 wastewater treatment. Mass flow rates of pharmaceutical compounds in influent and
 243 effluent streams were calculated by multiplying the measured concentrations in a given
 244 stream by the appropriate flow rate of that stream. Thus, the concentration of each
 245 pharmaceutical in the daily influent and effluent samples ($c_{influent}$ or $c_{effluent}$, [g/m³])
 246 was multiplied by the flow rate for that day (i.e. \dot{V}_l , [m³/day]) to give the mass of the
 247 pharmaceutical entering or leaving the plant that day (g/day) (i.e. daily mass load).
 248 Similarly, the concentration of pharmaceuticals in the treated sludge (c_{sludge} , [ng/g d.w.])
 249 was multiplied by the production rate of sludge (tons/day) to determine the mass of
 250 pharmaceuticals removed with the sludge (g/day). From these data, both removal from
 251 liquid-phase, $R_{Liquid\ phase}(\%)$, and overall removal (i.e. mass loss), $R_{Overall}(\%)$, of the target
 252 compounds were calculated according to the equations 3 and 4, respectively, and the results
 253 are presented in Figure 2:

$$254 \quad R_{Liquid\ phase}(\%) = 100 \times \frac{c_{influent} \times \dot{V}_l - c_{effluent} \times \dot{V}_l}{c_{influent} \times \dot{V}_l} \quad (6)$$

$$255 \quad R_{Overall}(\%) = 100 \times \frac{\dot{R}_{Overall}}{c_{influent} \times \dot{V}_l} \quad (7)$$

256

257

258 **3. Results and discussion**

259

260 **3.1. Occurrence of pharmaceuticals in wastewater and sludge**

261

262 In Table 2 are shown the frequencies of detection and the measured concentrations
263 of the pharmaceutical compounds detected in wastewater and sludge from the studied
264 WWTPs. Out of 43 analyzed pharmaceutical compounds, 32 were detected in influent, 29
265 in effluent and 21 in sludge samples. The analysis of samples from different campaigns of a
266 given plant showed variation in concentration levels, which is due to changes of the
267 composition of influent waters in different seasons, weather conditions and operational
268 conditions of the plant. For easier interpretation of the results, the concentrations of each
269 pharmaceutical are given as the median and maximum values of concentrations measured
270 for eight sampling campaigns. The concentrations lower than the method detection limits
271 are marked with n.d. (i.e. not detected).

272 According to the daily loads and population served by each plant, the amount of
273 pharmaceuticals disposed in these plants is estimated to be 5.6, 2.0 and 0.4 g/day/1000
274 equivalent inhabitants for WWTP1, WWTP2 and WWTP3, respectively (Figure 1). The
275 highest levels at the influent of all three WWTPs were observed for non-steroidal anti-
276 inflammatory drugs (NSAIDs) that were expected due to their high consumption. In
277 addition, topical application of the NSAIDs results in greater discharge of these compounds
278 in unmodified forms. This result is in fairly good agreement with previously reported
279 studies (Gracia-Lor et al., 2010, Miège et al., 2009). At the influent of the plants, this group
280 accounts for ca. 65% of all the therapeutic groups analyzed, as can be seen in the Figure 1.

281 Naproxen, ketoprofen and diclofenac were detected in all the samples in concentration
282 ranges 4.2-7.2 $\mu\text{g/L}$, 1.1-2.3 $\mu\text{g/L}$ and 0.4-1.5 $\mu\text{g/L}$, respectively. Ibuprofen and
283 acetaminophen were not included in the discussion because they yielded to high
284 concentrations which can be due to the strong matrix effect and/or to interactions that may
285 produce false identification and thus incorrect concentration values. Lower but still
286 significant levels of diuretics (~9%), lipid regulators (~9%) and beta-blockers (~6%) were
287 detected entering these WWTPs. Furosemide, bezafibrate, atenolol and anticonvulsant
288 carbamazepine were quantified in all the influent samples from the three WWTPs in
289 concentrations ranging from 0.4 to 1.4 $\mu\text{g/L}$.

290 The amount found in effluent or sludge depended on the removal efficiency of plant
291 and/or the properties of the compounds. As the influent concentrations give us information
292 about the consumption of the pharmaceuticals, the effluent and the sludge concentrations
293 are important from the environmental point of view, since the pharmaceuticals find their
294 way to the environment through discharges of treated waters to rivers, or disposal of sludge
295 to agricultural and forest land. In the effluent waters, the analgesics and antiinflammatories
296 were present in the highest percentage, i.e. 39%, followed by the lipid regulators (~37%)
297 and psychiatric drugs (~18%) (Figure1). The highest concentrations in the effluents of all
298 the WWTPs were found for naproxen, diclofenac and carbamazepine, and they ranged from
299 0.4 to 1 $\mu\text{g/L}$ depending on the compound and the removal efficiency of the plant. In the
300 treated effluent of WWTP2, ketoprofen, bezafibrate, atenolol and furosemide were detected
301 in much higher concentrations (0.7, 0.4, 0.4 and 0.9 $\mu\text{g/L}$, respectively) than in the other two
302 plants. Analysis of sludge samples showed the presence of 21 out of 43 analyzed
303 pharmaceuticals, where diuretics accounted for ca. 19%, antibiotics ca. 18% and lipid
304 regulators ca. 16% of all the pharmaceuticals analyzed. Hydrochlorthiazide, furosemide,

305 atorvastatine, clarithromycin, carbamazepine and diclofenac were ubiquitous in samples
306 from all three WWTPs, in concentrations from 30 to 60ng/g. On the other hand, β -blockers,
307 β -antagonists and histamine H₂-antagonists were found in very low concentrations in
308 sludge. The total loads of analyzed pharmaceuticals that leave the plants unmodified
309 (including sludge and effluent water) were calculated to equal 1.1, 0.9 and 0.1 g/day/1000
310 equivalent inhabitants for WWTP1, WWTP2 and WWTP3, respectively, of which only 3-
311 9% (depending on the plant) was retained by sludge (Figure 1). The amount of
312 pharmaceutical compounds detected in this study exiting the plants is not of great concern
313 if we compare it with the results from some other studies done in this field (Zorita et al.,
314 2009; Castiglioni et al., 2005).

315

316 **3.2. Overall removal of pharmaceuticals during wastewater treatment**

317

318 The daily mass loads of target compounds in wastewater influent and effluent, and
319 in sludge, in g/day, were calculated as explained previously, and these values were used for
320 the estimation and the comparison of the liquid phase and the overall removal rates (Figure
321 2). Considering the fact that pharmaceuticals are grouped by the therapeutical applications
322 for which they are used and not on the basis of their physico-chemical similarity, their
323 removal during treatment is expected to be diverse. Here the term removal refers to the
324 conversion of a pharmaceutical to a compound different than the analyzed one (i.e. the
325 parent compound). Thus, the overall removal refers to all the losses of a parent compound
326 produced by different mechanisms of chemical and physical transformation, biodegradation
327 and sorption to solid matter.

328 High liquid-phase removal rates for some compounds (i.e. lipid regulator
329 fenofibrate and hystamin H2 receptor antagonist famotidine) would suggest very good
330 removal of these compounds during the wastewater treatments. But, as shown in the Figure
331 2, only a certain percent of the total mass input is really lost during the treatments (overall
332 removal). The rest was accumulated in sludge or discharged with the effluent. Sorption of
333 fenofibrate, atorvastatine, diazepam and clarithromycin contributed to the elimination from
334 the liquid phase with more than 20% related to the amount of these compounds at the
335 influent. This finding clearly indicates the importance of the analysis of sludge when
336 studying wastewater treatment performances. Since many of the analyzed compounds were
337 found in the sludge samples, the overall removal rate was the parameter used to compare
338 the removal performances of the studied treatment plants.

339 In general, the removal rates varied strongly without evident correlation to the
340 compound structure, as can be seen in the Figure 2. The antihypertensive enalapril and
341 NSAIDs ketoprofen and naproxen were removed in all the three cases with very good
342 removal efficiency (>80%) and they did not accumulate in sludge. Similar removal of these
343 compounds from liquid phase, under conventional treatment conditions, was observed in
344 various studies on this topic (Zorita et al., 2009; Gros et al., 2010; Sim et al., 2010;
345 Lishman et al., 2006). But then, the most analyzed anticonvulsant carbamazepine showed
346 very low removal (<25%) regardless of the treatment applied. The results concerning its
347 persistence and ubiquitous occurrence match with those from previous studies (Joss et al.,
348 2005; Radjenovic et al., 2007; Pérez et al., 2007). No significant overall removal during the
349 studied treatments (<30%) was observed for antibiotics trimethoprim and metronidazole,
350 NSAIDs mefenamic acid, hystamin H2 receptor antagonist famotidine and benzodiazepine
351 lorazepam. A benzodiazepine diazepam and antimicrobial chloramphenicol were detected

352 in concentrations close to their corresponding LOQs thus no reliable conclusion could be
353 made on their behaviour.

354 Cholesterol lowering statin drugs pravastatin and mevastatin, antibiotics
355 sulfamethazine and metronidazole, β -blockers metaprolol and timolol, β -antagonist
356 salbutamol were not accumulated in sludge and they showed a variety of removal rates
357 between 30 and 80%. Inconsistent overall removal was also observed for NSAIDs
358 diclofenac and indometacin, hystamin H₂ receptor antagonists cimetidine and ranitidine,
359 and diuretic furosemide. It seems that for the mentioned compounds, removal was mainly
360 influenced by operational conditions and treatment technology used. Comparing to the
361 other two plants, WWTP1 offers much better removal for the majority of the analyzed
362 compounds (Figure 2). This activated sludge plant featured by a tertiary treatment in
363 WWTP1 improves the removal of diclofenac to 60%, while in the other two plants removal
364 is much lower (<24%). Low removals of diclofenac were already reported in some
365 publications on this topic (Quintana et al., 2005; Kimura et al., 2007; Cirja et al., 2008)
366 imputed its persistence to the presence of chlorine group in the molecule. Some studies on
367 removal during wastewater treatment showed no influence of solid retention time on the
368 removal of diclofenac (Clara et al., 2005; Kreuzinger et al., 2004; Lishman et al., 2006).
369 Furosemide, pravastatin, and ranitidine that were eliminated with removal ca. 80% and
370 60% in WWTP1 and WWTP3, respectively, marked very low (ca.30%) removal rates in
371 WWTP2. Better performances of WWTP1 and WWTP3 may be due to longer both
372 hydraulic and solid retention times which are proved to influence the elimination of most of
373 the pharmaceuticals during sewage treatment (Clara et al., 2005; Göbel et al., 2007; Reif et
374 al., 2008; Suárez S et al., 2005). If a compound spends more time in reactors then bacteria

375 growth is promoted so biological transformation may occur to a greater extent (Reif et al.,
376 2008).

377 The negative values of removal rates (omitted in the Figure 2) refer to an increase in
378 the concentration of an analyzed parent compound during treatment. This phenomenon of
379 “negative removal” for some compounds was already reported in the literature (Gros et al.,
380 2009; Wick et al., 2009; Joss et al., 2005). Hydrochlorothiazide was not detected in influent
381 neither effluent water samples, but it was detected in sludge. This was not at all expected
382 according to its low logP and the fact that >95% of the dose of this pharmaceutical is
383 excreted unchanged (EMEA/CHMP/471165/2009). Lipid-regulating agent gemfibrozil was
384 detected in higher concentration in the effluent than in the influent water samples. Similar
385 was observed for macrolide clarythromycin, anti-diabetic glibenclamide, lipid regulators
386 fenofibrate and atorvastatin, as well as for carbamazepine in one of the plants, which
387 yielded higher concentration levels at the exit of a plant (i.e. including effluent and sludge)
388 than at its entrance. This could be explained by the formation of unmeasured products of
389 human metabolism and/or transformation products (e.g. glucuronide conjugate, methylates,
390 glycinates etc.) that passing through the plant convert back to the parent compounds. This
391 can be considered as a reasonable assumption since the metabolites and some derivatives of
392 the mentioned compounds are well-known (e.g. hydroxy and epoxy-derivatives of
393 carbamazepine; 4-trans-hydroxy and 3-cis-hydroxy derivatives of glibenclamide; ortho- and
394 parahydroxylated derivatives of atorvastatine; gemfibrozil acyl glucuronide etc.) (Miao et
395 al., 2005; Shipkova et al., 2005; Aviram et al., 1998). Gobel et al. (Göbel et al., 2007)
396 proposed gradual release of the macrolides (e.g. clarithromycin) from feces particles during
397 biological treatment as an explanation for the possible negative removal rates for these
398 antibiotics. During complex metabolic processes in human body and bio-chemical in

399 wastewater treatment, various scenarios of transformation from parent compound to
400 metabolite and derivatives and vice versa can occur. These metabolites can be just as active
401 as their parent compounds (<http://www.rxlist.com>). Therefore, the occurrence of
402 metabolites and transformation products and pathways should be included in the future
403 studies in order to obtain accurate information on removal of pharmaceuticals during
404 treatment and to determine treatment plant capabilities.

405

406 **4. Conclusion**

407

408 This work presents the results obtained in a two year study on the occurrence and
409 fate of the selected pharmaceuticals during conventional wastewater treatment. Out of 43
410 analyzed pharmaceuticals, 32 compounds were detected in wastewaters in concentrations
411 ranging from low ng/L to a few $\mu\text{g/L}$ (e.g. antiinflammatories). The variety of the compounds
412 detected in effluent wastewaters indicates that WWTP outlets are important contributors of
413 pharmaceuticals in the aquatic environment. This study showed that 21 of 43 analyzed
414 compounds accumulated in sludge in concentrations up to 100ng/g. Thus the disposal of
415 sludge to the agricultural land can be another mechanism for the reintroduction of these
416 micro-contaminants into the environment through the WWTPs. For this reason the results
417 of this and similar studies can be considered as very useful for rough estimations of the
418 magnitude of the pharmaceuticals releases from WWTPs into the environment. A simple
419 mass balance involving data for influent and effluent wastewater and sludge, for the
420 pharmaceuticals in the three monitored WWTPs, was employed for calculation of the
421 removal rates. Varying removals and no evident pattern in behavior were observed even for
422 the compounds belonging to the same therapeutic group. Significantly low and even

423 negative removals were observed for some compounds (carbamazepine,
424 hydrochlorothiazide etc.) which can be result of the formation of unmeasured
425 transformation products that passing through the plant convert back to the parent
426 compounds. There are many factors that should be considered while studying wastewater
427 treatment performances. The screening of the metabolites and some other transformation
428 products (such as conjugates: glucuronides, methylates etc.) should be naturally included in
429 the study of wastewater treatment processes. What is clear from the results is that, even
430 though the WWTPs meet the regulatory requirements for wastewater treatment (Directive
431 91/271/EEC), they are only moderately effective in removing pharmaceutical compounds.
432 This is an issue of great importance especially when attempting to reuse wastewater and
433 dispose sludge to agricultural areas and landfills.

434

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446

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633

Table 1. Characteristics of the studied wastewater treatment plants (WWTPs)

	Type of treatment	Designed Treatment Capacity (m ³ /day)	Average Flow Treated in 2008 (m ³ /day)	Population Equivalent	Sludge Treatment	Disposal of Sludge	Sludge produced in 2008 (t/year)
WWTP 1	Biological + Tertiary	47500	25000	74000	Composting	Disposal to soil; Agricultural usage	9000 (1800 d.m.)
WWTP 2	Biological	35000	26000	170000	Anaerobic digestion	Disposal to soil; Incineration	8500 (2000 d.m.)
WWTP 3	Biological with Phosphorus and Nitrogen Removal	25000	21000	400000	Anaerobic digestion + Drying	Controlled disposal to landfill	11400 (2900 d.m.)

*d.m. dry matter (dry weight)

Table 1. Characteristics of the studied wastewater treatment plants (WWTPs)

A) Treatment characteristics

	Type of treatment	HRT (h)	SRT (days)	Designed Treatment Capacity (m ³ /day)	Average Flow (m ³ /day)	Population Equivalent	Sludge treatment	Disposal of sludge	Sludge production (t/year)	Dry matter (t/year)	Organic matter (%)
WWTP1	Biological + Tertiary	26-40	10	47500	25000	74000	Composting	Disposal to soil; Agricultural usage	9000	1800	75
WWTP2	Biological	20	6	35000	26000	170000	Anaerobic digestion	Disposal to soil; Inceneration	8500	2000	65
WWTP3	Biological with P and N removal	40	16	25000	21000	400000	Anaerobic digestion + Drying	Controlled disposal to landfill	11400	2900	53

B) Wastewater and sludge characteristics

	Wastewater													Sludge					
	SS _{Influent} (mg/L)	SS _{Effluent} (mg/L)	BOD _{5In} (mg/L)	BOD _{5Out} (mg/L)	COD _{In} (mg/L)	COD _{Out} (mg/L)	N _{tIn} (mg/L)	N _{tOut} (mg/L)	P _{tIn} (mg/L)	P _{tOut} (mg/L)	T _{effluent} (°C)	pH _{Influent}	pH _{Effluent}	N _{tSludge} (%)	N _{amoniium} (%)	N _{organic} (%)	P (P2O5) (%)	K (K2O) (%)	pH _{Sludge}
WWTP1	191	43	175	19	393	82	39	25	6	4	n.d.	7.7	7.3	5.4	1.2	4.2	3	0.3	6.5
WWTP2	330	20	390	14	700	85	70	42	8	3	20 ± 6	n.d.	7.2	5.9	2.9	2.9	5	0.3	6.4
WWTP3	750	10	1130	6	1800	36	126	11	16	1	22 ± 5	7.5	7.2	5.1	1.1	4.1	3.6	0.2	7.6

SPM - Suspended particulate matter

BOD5 - Biochemical Oxygen Demand

COD - Chemical Oxygen Demand

Nt - Total Nitrogen

Pt - Total Phosphorus

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Table 2. Frequency of detection (%) and median and maximum (max) concentrations of pharmaceuticals detected in wastewater influent (WWI), effluent (WWE) and sewage sludge from the studied wastewater treatment plants (WWTP1, WWTP2 and WWTP3) during 8 sampling campaigns

Compounds	Frequency of detection, %			WWTP 1						WWTP2						WWTP3					
	WWI	WWE	Sludge	C Influent, ng/L		C Effluent, ng/L		C Sludge, ng/g		C Influent, ng/L		C Effluent, ng/L		C Sludge, ng/g		C Influent, ng/L		C Effluent, ng/L		C Sludge, ng/g	
				Median	Max	Median	Max	Median	Max	Median	Max	Median	Max	Median	Max	Median	Max	Median	Max	Median	Max
Ketoprofen	100	54	0	2244	3301	160	340	n.d.	n.d.	2270	6007	690	948	n.d.	n.d.	1100	1720	70	80	n.d.	n.d.
Naproxen	100	88	0	7129	8862	455	1446	n.d.	n.d.	4802	10150	1126	2624	n.d.	n.d.	4161	5545	105	307	n.d.	n.d.
Diclofenac	92	100	100	1532	1709	456	743	61	97	1090	1674	785	1100	23	36	385	1250	336	900	40	75
Indomethacine	65	58	0	166	997	74	495	n.d.	n.d.	175	873	128	622	n.d.	n.d.	74	187	43	440	n.d.	n.d.
Mefenamic acid	54	77	83	130	212	58	113	19	81	68	132	20	30	15	21	50	50	10	15	29	56
Bezafibrate	100	100	100	436	1969	80	240	17	23	503	1346	441	500	18	27	204	583	48	100	3.1	7.4
Fenofibrate	42	0	79	27	30	n.d.	n.d.	6.7	65	5.2	25	n.d.	n.d.	22	45	9.1	9.1	n.d.	n.d.	16	21
Gemfibrozil	38	58	50	107	135	378	525	2.6	3.8	42	145	139	1772	4.2	6.6	283	1040	31	45	2.3	3.2
Atorvastatin	100	77	96	65	159	15	64	20	70	79	180	53	395	34	56	22	110	5.4	5.4	33	46
Pravastatin	73	65	0	179	558	22	69	n.d.	n.d.	123	710	68	619	n.d.	n.d.	49	50	19	92	n.d.	n.d.
Mevastatin	12	8	0	1353	1353	476	476	n.d.	n.d.	208	208	287	287	n.d.	n.d.	135	135	n.d.	n.d.	n.d.	n.d.
Diazepam	54	54	88	7.4	8.8	3.5	5.0	6.5	9.3	3.7	7.1	5.1	7.4	6.1	11	3.2	3.2	5.2	5.7	4.5	7.0
Lorazepam	81	85	79	64	70	50	75	11	15	93	126	64	208	10	19	49	160	31	116	8	11
Carbamazepine	100	100	100	782	949	539	705	29	68	664	814	509	665	23	35	327	561	367	518	31	46
Clarithromycin	73	85	83	86	113	33	55	55	91	57	501	50	184	40	75	44	333	30	116	44	54
Cimetidine	100	69	88	210	534	10	10	7	12	140	207	80	132	6.9	12	41	185	14	47	5.6	8.7
Ranitidine	92	88	92	113	456	9	63	8	19	221	840	179	401	4.6	6	127	323	34	76	4.6	20
Famotidine	19	8	96	42	45	n.d.	n.d.	13	15	19	21	16	18	6.6	14	14	14	n.d.	n.d.	7.5	27
Sulfamethazine	58	65	33	6.1	6.1	3.2	3.2	n.d.	n.d.	10	24	1.7	8.1	n.d.	n.d.	20	586	12	195	12	23
Trimethoprim	100	96	88	155	237	42	147	30	36	176	645	101	255	12	80	56	95	29	86	12	20
Metronidazole	62	62	0	47	392	30	187	n.d.	n.d.	104	285	118	295	n.d.	n.d.	15	19	13	13	n.d.	n.d.
Chloramphenicol	12	46	0	23	23	17	21	n.d.	n.d.	4.0	4.0	4.0	14	n.d.	n.d.	n.d.	n.d.	2.3	2.3	n.d.	n.d.
Atenolol	100	100	88	490	1451	129	574	9	17	1195	1436	383	1160	7.8	28	382	1310	63	139	4.3	8.1
Sotalol	65	58	54	88	859	49	147	12	20	72	157	63	92	9.4	23	86	193	42	65	9.3	16
Metoprolol	35	62	0	131	196	82	141	n.d.	n.d.	15	17	10	35	n.d.	n.d.	n.d.	n.d.	3.6	6.9	n.d.	n.d.
Timolol	42	65	0	10	10	4.6	6.7	n.d.	n.d.	11	12	7	10	n.d.	n.d.	7.4	7.4	4.2	4.8	n.d.	n.d.
Nadolol	100	69	54	20	48	5.4	7.6	2.0	2.3	22	82	13	78	3.2	6.3	7.8	17	n.d.	n.d.	6.4	7.0
Salbutamol	69	58	0	44	67	5.8	24	n.d.	n.d.	45	48	19	23	n.d.	n.d.	12	15	6.7	10	n.d.	n.d.
Enalapril	96	46	0	165	567	1.2	10	n.d.	n.d.	344	1309	6.5	1041	n.d.	n.d.	214	773	8.5	8.5	n.d.	n.d.
Glibenclamide	85	65	92	32	100	18	38	20	88	60	200	58	162	19	32	10	103	11	100	34	49
Furosemide	100	96	83	1371	1530	142	491	36	75	1374	2437	865	1371	24	52	865	925	212	443	43	54
Hydrochlorothiazide	0	0	100	n.d.	n.d.	n.d.	n.d.	37	53	n.d.	n.d.	n.d.	n.d.	39	65	n.d.	n.d.	n.d.	n.d.	32	42

Table 2. Frequency of detection (%) and limits of quantification (LOQ) of pharmaceuticals detected in wastewater influent (WWI), effluent (WWE) and sewage sludge from the studied WWTPs during 8 sampling campaigns

Compounds	Frequency of detection, %			LOQ (ng/L)		LOQ (ng/g)
	WWI	WWE	Sludge	WWI	WWE	Sludge
Ketoprofen (KTP)	100	54	0	13	7.0	1.3
Naproxen (NPR)	100	88	0	21	3.0	0.9
Diclofenac (DCL)	92	100	100	4.0	4.0	2.0
Indomethacine (INM)	65	58	0	3.0	2.0	1.0
Mefenamic acid (MFA)	54	77	83	16	5.0	0.4
Bezafibrate (BZF)	100	100	100	4.0	0.4	0.4
Fenofibrate (FNB)	42	0	79	0.5	0.5	2.5
Gemfibrozil (GMB)	38	58	50	3.0	1.0	1.7
Atorvastatin (ATR)	100	77	96	4.0	2.0	2.5
Pravastatin (PRV)	73	65	0	25	9.0	2.4
Mevastatin (MVS)	12	8	0	2.0	2.0	4.5
Diazepam (DZP)	54	54	88	3.0	1.2	4.1
Lorazepam (LRZ)	81	85	79	7.0	4.0	5.1
Carbamazepine (CBZ)	100	100	100	2.0	2.0	0.2
Clarithromycin (CLR)	73	85	83	5.0	4.0	7.1
Cimetidine (CMTD)	100	69	88	0.6	0.4	0.2
Ranitidine (RNTD)	92	88	92	3.0	2.0	0.3
Famotidine (FMTD)	19	8	96	1.0	0.7	0.1
Sulfamethazine (SLFM)	58	65	33	2.0	1.0	0.8
Trimethoprim (TRM)	100	96	88	1.0	0.4	0.6
Metronidazole (MTR)	62	62	0	6.0	0.7	5.6
Chloramphenicol (CHLR)	12	46	0	2.0	0.6	0.2
Atenolol (ATN)	100	100	88	9.0	9.0	0.7
Sotalol (STL)	65	58	54	5.0	2.0	0.4
Metoprolol (MTP)	35	62	0	2.0	2.0	1.2
Timolol (TML)	42	65	0	0.3	0.3	0.9
Nadolol (NDL)	100	69	54	0.8	0.2	0.3
Salbutamol (SLB)	69	58	0	0.3	0.2	0.3
Enalapril (ENL)	96	46	0	5.0	0.7	0.4
Glibenclamide (GLB)	85	65	92	5.0	4.0	3.5
Furosemide (FRS)	100	96	83	4.0	2.0	1.0
Hydrochlorothiazide (HCRT)	0	0	100	13	6.0	0.5

Figure 1. Daily mass loads of different therapeutic groups at the influent and effluent, and in the sludge from the studied WWTPs

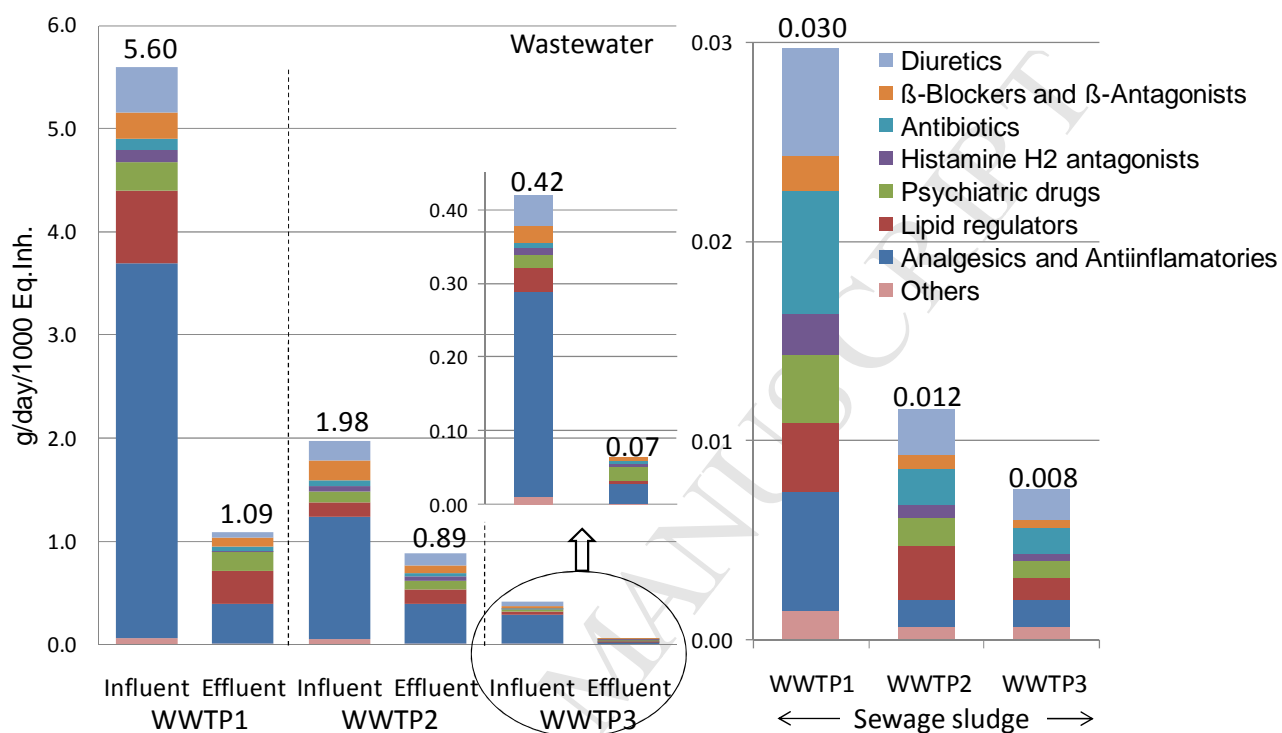


Figure 1. Schematic diagram of the studied wastewater treatment plants.

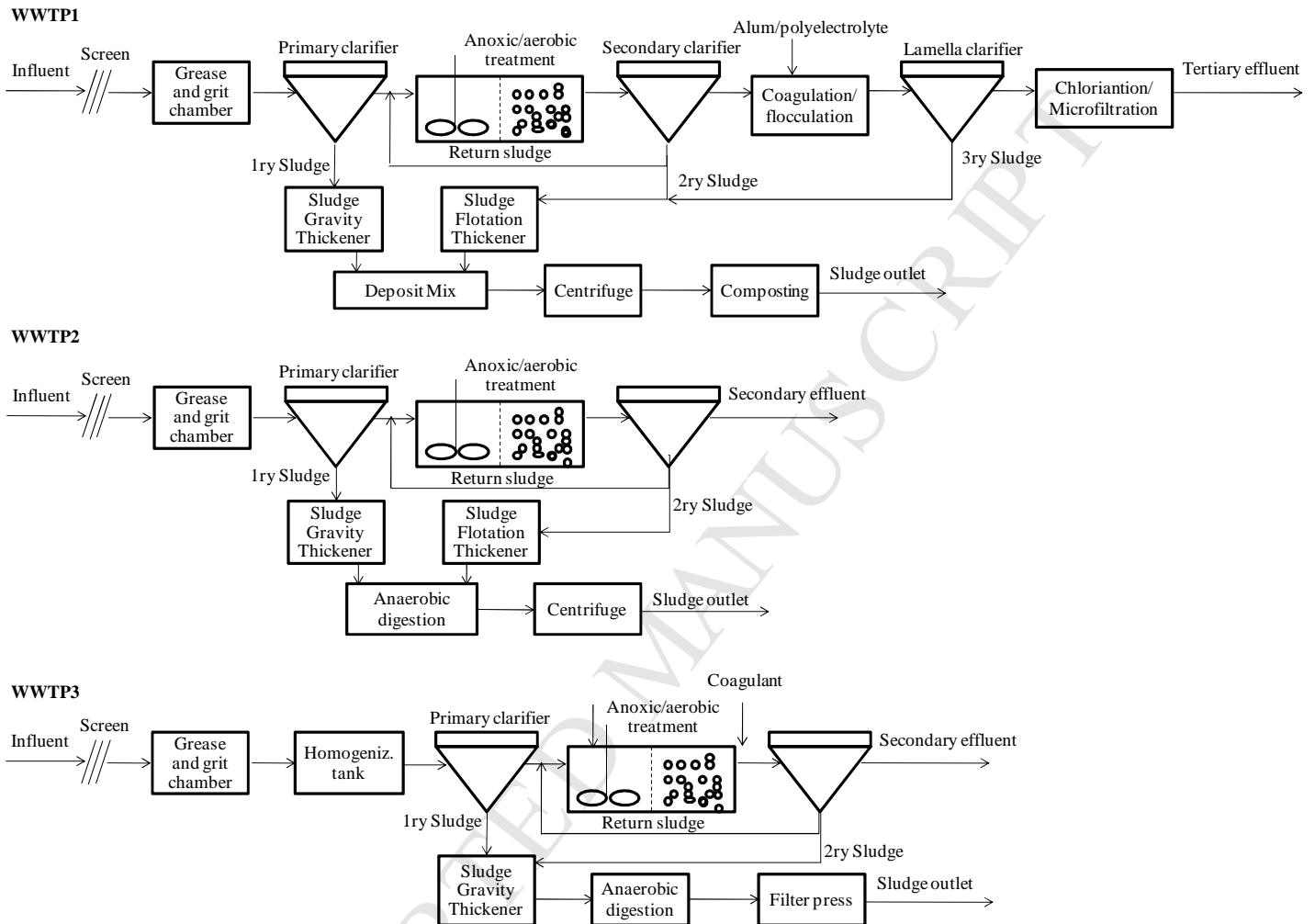


Figure 2. Normalized mass loads of the selected pharmaceuticals entering the studied WWTPs

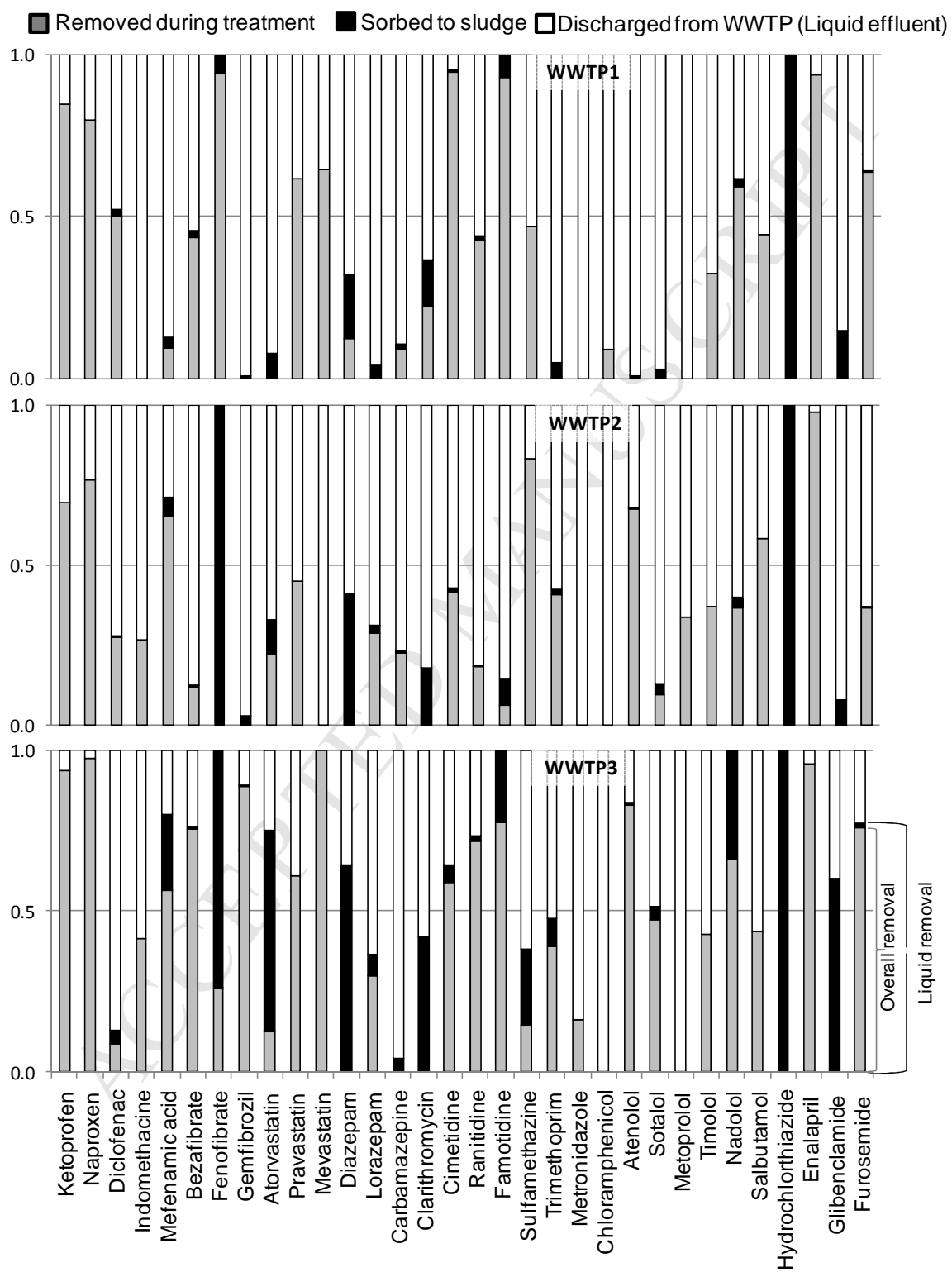


Figure 2. Box plots of concentration ranges (Min (-), P 0.25, Median, P 0.75 and Max (▲) of the pharmaceuticals detected in wastewater influent (IN), effluent (OUT) and sewage sludge from the studied wastewater treatment plants (WWTP1, WWTP2 and WWTP3) during 8 sampling campaigns (compound abbreviations are indicated in Table 2)

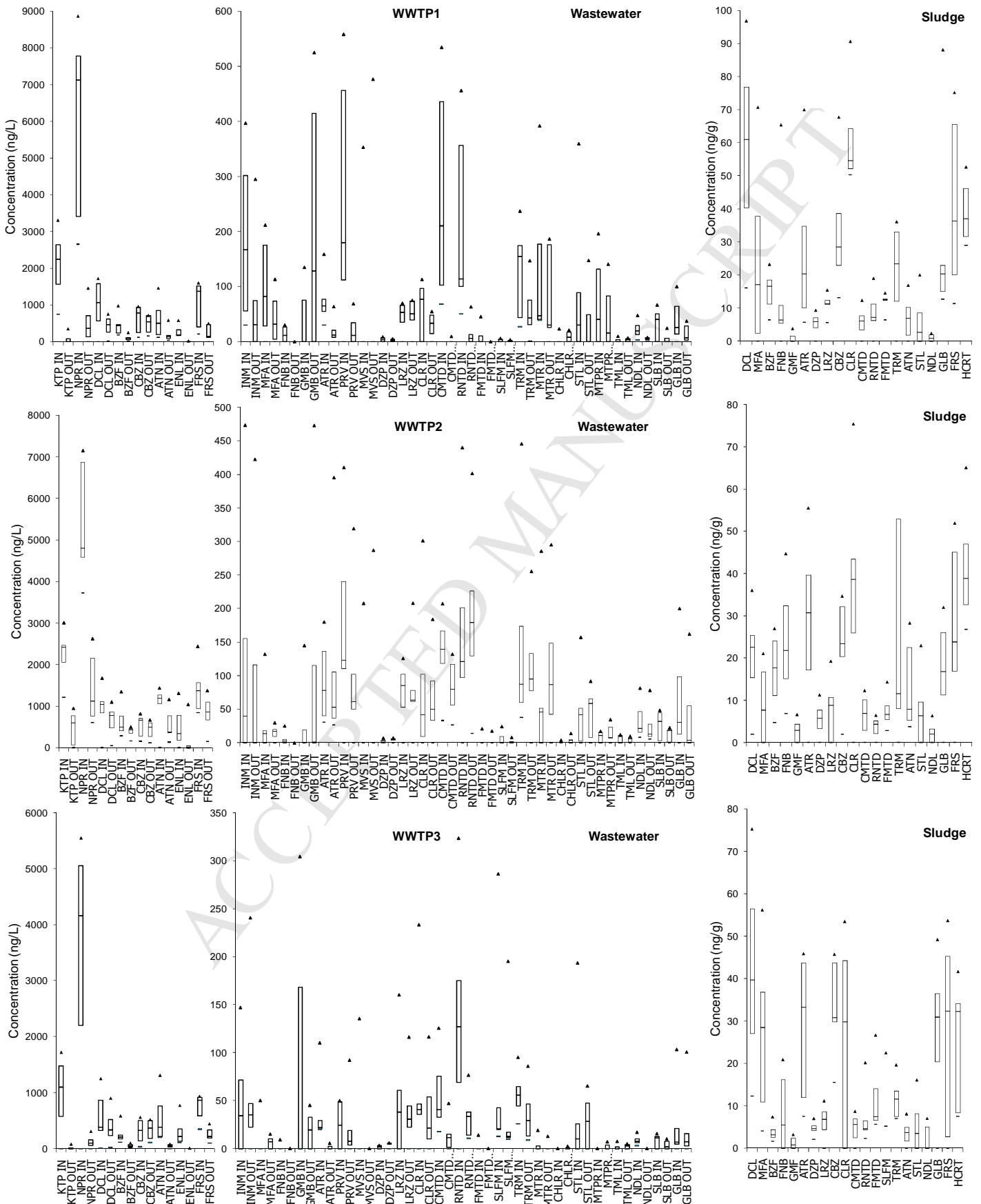


Figure 3. Daily mass loads (g/day per 1000 eq.inh.) of different therapeutic groups at the influent and effluent, and in the sludge from the studied WWTPs

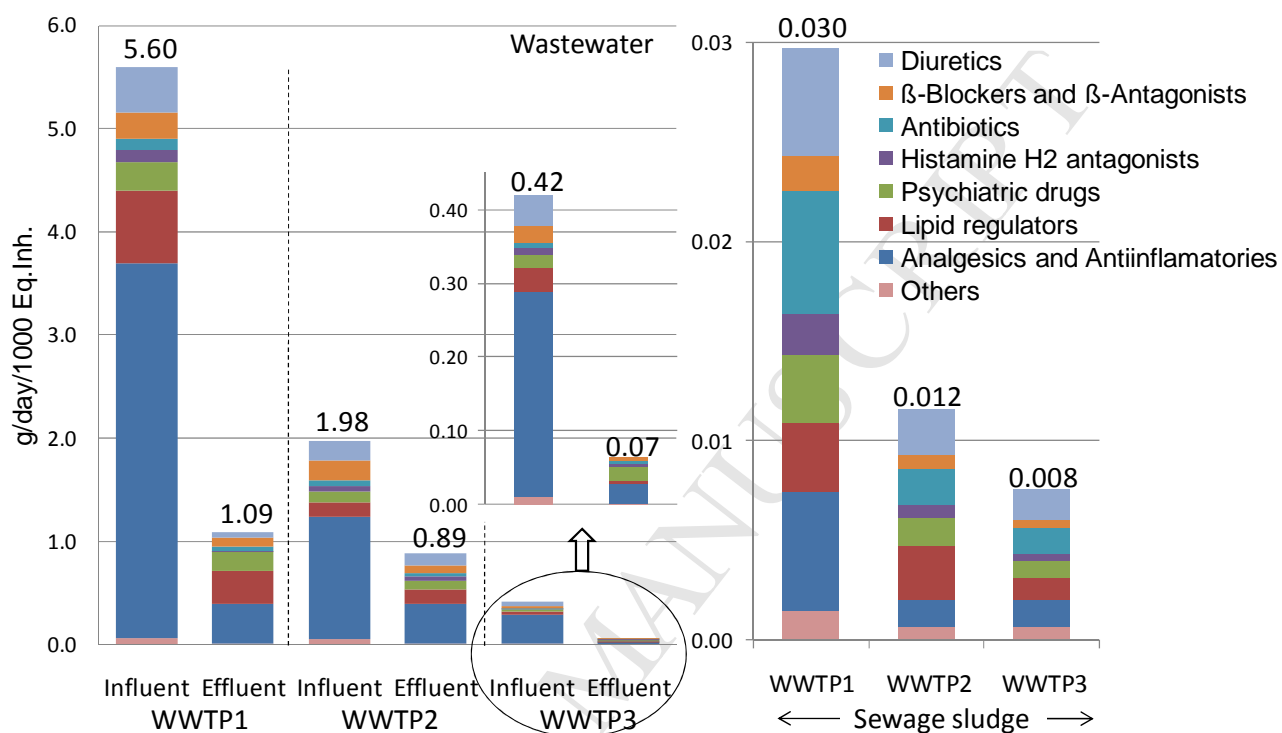


Figure 4. Normalized mass loads of the selected pharmaceuticals entering the studied WWTPs (i.e. fraction discharged with effluent, sorbed to sludge, and removed during treatment (overall removal rate))

